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This research is done after my participating with \*  
erection team in executing SMI Melt shop with  
capacity of 50000 Ton per year in Syria in 2013.

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## **Abstract**

Since I joined E.I.S.C which is an erection company in ١٩٧٢ in Syria as senior piping engineer and static equipment installation, the company executed a large Melt Shop of capacity ٧٠٠٠٠ Ton per year in Syria .This Melt Shop is manufactured by Italian company Danieli ,also Danieli supervised the erection procedure step by step and under their standard and also as per the international STD like ANSI,ASME,API,DIN,etc. I acquired good experience in pipe fabrication in, hydraulic system, water supply, gases, lime, etc. and their relative equipments. Therefore I found the hydraulic system as important part from the erection procedure to be worth full discussed and highlighted because it was very complex and got very special way in erection and fabrication . This document is reliable for any hydraulic system installation and pipe fabrication in a safe procedure.

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## **HYDRAULIC POWER SYSTEMS (In Melt Shop/DanieliSTD )**

### **SCOPE**

This specification covers the hydraulic power systems required for various units in SMI Melt Shop in Syria as per DanieliSTD. And as I participated in the erection company of this Melt Shop as a piping senior supervisor and the installation of various equipments, the hydraulic system was one of most interesting system that should be taken into consideration, therefore this research is submitted.

The term “Hydraulic power systems” referred herein generally covers the following:

- Hydraulic power units (reservoirs, pumps recirculating units, etc.)
- Valve stands
- Accumulator stands
- Interconnecting pipe work

This general specification does not cover on board of machine pipework and associated equipment.

The hydraulic power systems covered herein are intended for actuation of components of various production and ancillary equipment in the steel complex to achieve specific functions such as application of pressure/force /torque, generation of linear or rotary motion, control flow of fluids in pipes and ducts etc.

The design and construction of the hydraulic power systems shall be suitable in every way for the service intended and shall be oriented towards maximizing interchangeability and to minimize maintenance. Each system shall be complete and it will include accessories essential for proper installation, operation and maintenance, irrespective of whether such systems are mentioned in the Technical and General Specification document.

## **STANDARDS**

The hydraulic power systems shall be designed, manufactured, erected, tested and commissioned as per the standards laid down in this specification. Detailed instructions on such aspects as are not indicated herein shall be as per the codes and practices adopted by the ISO and EN standards.

## **DESIGN BASIS**

The design should ensure that the components of the hydraulic power systems are compatible with the hydraulic fluid selected at operating conditions in the plant under atmospheric condition. In selecting the hydraulic fluid the operating temperature of the systems shall be given careful consideration.

## **HYDRAULIC CIRCUITS**

Each hydraulic circuit shall be designed to minimize surge pressure. Suitable accumulator of adequate size shall be used to withstand maximum rate of surge pressure rise as well as the peak surge pressure. All components shall be capable of withstanding the peak surge pressure. Each hydraulic circuit shall be designed to minimize generation of heat in the system by adequately sizing.

The pipework and valves and by reducing bends and restrictions but without sacrificing the functional efficiency of the system. Coolers shall be incorporated in the system to remove excess heat

in order to stabilize required viscosity. Design of each circuit shall be such as to achieve quick response to functional needs, economic operation of the system, minimum maintenance as well as shall ensure safety of the staff and equipment. The hydraulic system shall be designed taking into account the maximum pressure encountered. Each circuit shall incorporate a reservoir of adequate capacity, pumping equipment, filters to eliminate undesirable particles of contaminants. Pipework, accessories and hoses, adequate cooling system to cool the hydraulic fluid where required, Accumulators, all valves and all necessary audio visual alarms, unless otherwise specified hydraulic equipment located in

unattended areas, basements, etc. shall have remote control facilities to ensure safety of the main equipment served.

## **EQUIPMENT**

### **RESERVOIRS**

Reservoir shall have a working volume adequate to contain all the fluid that will return from the system, maintain the fluid level within adequate working height limits during operation and feed the system for a minimum of three minutes at the rated pumping capacity. The working volume of the reservoir shall form about 10 per cent to 15 per cent of the total volume of the reservoir, the balance being air space.

The minimum fluid level shall be at least 100 mm above the upper most point of the suction pump. The reservoir shall be designed and constructed to prevent entry of foreign matter, including water. Reservoirs shall be fabricated from **structural steel** of adequate strength and thickness. Cast reservoirs shall not be used. Carbon steel reservoirs shall be painted according to Danieli. When HFC fluid is used, stainless steel reservoir is suggested.

All reservoirs shall have provisions for oil filling and air breathing. Filler holes shall be provided with caps or covers. A breather hole shall be provided and shall be protected by an air filter. The air filter shall be of sufficient capacity to maintain approximate atmospheric pressure even at maximum demands of the hydraulic system and shall be so located as to be unaffected by splashes liquids and exit of reservoir fluid.

The reservoir shall be equipped with a fluid visual level indicator preferably located near the filler connection. Low level alarms shall be provided on each reservoir, unless specifically. Visual level shall be provided with indicators showing high and low

levels. Both the intake and return pipe shall be brought down below the minimum working fluid level so as not to cause cavitations or aeration. Suitable provision shall be made for efficient cleaning of reservoir. A suitable opening with cover shall be provided, shall be suitable for a man to go into the tank. An accessible means shall be provided to empty the reservoir. The reservoir bottom shall be

shaped to facilitate emptying and cleaning by providing minimum slope at the bottom.

## **PUMPS**

Pumps shall be designed to meet the system operating pressures according to manufacturer indications. Pump motors shall be adequate to operate of the system. Unless otherwise specified the main pumps shall be provided with at least one stand-by unit for each group. The stand-by pump shall be connected to the circuit and kept ready for operation. Direct-coupled pumps shall be securely mounted in a manner to assure alignment under normal operating conditions. The couplings and other power transmission equipment shall be designed as per General Specification for Mechanical Machinery. The following information shall be permanently shown on metallic nameplates on each hydraulic pump:

- a) Manufacturer's name and address
- b) Model and/or serial number
- c) Maximum pressure

The direction of rotation of each pump shall be clearly indicated on the pump where it can be readily seen.

## **VALVES**

All valves shall be sized to meet the intended flow rates, consistent with low pressure drop (according to manufacturer indications).

Valves and other controls shall be mounted on panels or valve stands or on the related power unit.

All directional valves shall be sub-plate mounted. Where practical, directional valve of large capacity shall be hydraulic pilot operated.

If air pilot valves are used they shall have speed control plugs on air exhaust. Sub-plate "O" ring mounted valves shall have locating pins or non-symmetrical bolt holes for fool proof mounting.

Solenoid operated valves shall be designed, constructed and installed to eliminate destructive hammering of the solenoid or spool. Solenoid operated valves shall incorporate the following features:

- a) Suitably sealed solenoid enclosure to prevent the entrance of splashing liquids and airborne contamination.

- b) Non-dented manual over-rides which can be operated without removing the solenoid covers but which cannot be operated accidentally.
- c) Solenoids shall be continuous duty type
- d) Solenoid indicating lights
- e) Solenoid valve shall be equipped with plug type connectors (DIN standard) for ease of replacement and maintenance. All hydraulic valves, accessories and devices shall be plainly identified as to the item shown on the diagram. Such identification shall be shown on a tag mounted adjacent to the component. All valves such as directional valves and flow control valves (operated manually, pneumatically, electrically, hydraulically or by any combination of these actuators),

Relief valves, check valves and special valves such as brake valves, locking valves, pressure control valves, prefill valves, popped valves, pressure sequence valves, servo-control valves etc. shall have frame sized ports, connection etc. conforming to ISO/CETOP standards.

### **ACCUMULATORS**

The accumulator shall conform to the European directive PED for pressure vessels unless otherwise specified.

Design pressure of accumulators shall be at least that of the circuit.

### **Marking**

The following particulars shall be shown in a permanent and readily visible form on each hydraulic accumulator:

- The manufacturer's/supplier's name and brief address
- The manufacturer's /supplier's product identification
- The rated pressure
- Date of manufacture (month/year)
- Manufacturer's serial number
- Total shell volume in liters
- Allowable temperature range in degrees Celsius

The following identification shall be given on the accumulator or on a label on the accumulator:

- "Caution – Pressurized vessel. Discharge prior to disassembly"
- Gas pre-charge pressure

- "use only ..... "(Pre-charge medium, e.g. nitrogen)

### **COOLERS AND HEATERS**

Coolers shall be tube or plate type exchangers and shall be used where normal operation of the system would raise the temperature of the fluid to over 60°C. The cooling medium may be air or water. Tube heat exchangers, plate heat exchangers and finned tubes shall be designed as per supplier's standards.

Heaters shall be used if the viscosity of the hydraulic fluid in cold seasons would affect the pump operation adversely. The heaters shall preferably be of electrical type, having a heating intensity of not more than 1 watt per sq. cm for stagnant oil and 3 watts per sq. cm for flowing oil. This limitation is to prevent cracking of the hydraulic fluid due to local overheating.

Electrical heaters shall preferably be of cartridge type, suitable for mounting in reservoir or pipe and shall be thermostatically controlled. Heat exchangers shall be protected against excessive pressure or pressure surges by suitably providing pressure safety. Where HFC fluids are used, the temperature of the fluid shall be controlled so as not to exceed 60°C.

### **FILTERS**

Filters shall be provided for continuous removal, from the hydraulic fluid, of contaminants which are likely to cause malfunction of valves and actuators. Adequate filtration shall be provided in accordance with manufacturer's recommendations. The filtration capacity shall be selected in order to maintain the following contamination level on the systems according to ISO 4406 class (NAS 1638):

- Standard 19/17/14 (NAS 8)
- Servo valves 16/14/11 (NAS 6)

These filters shall have differential pressure switch connection and will give also visual indication of clogging. If any hydraulic circuit element demands for extremely fine filtration a separate filter suitable for that component shall be used for system economy.



Pressure line, return line and circulation line filters shall be so constructed and installed that the filter element can be changed for cleaning or replacement without disturbing the piping. Component parts of filter in contact with hydraulic fluid shall be compatible with the fluid and resistant to the corrosive effects of moisture.

### **SEALING DEVICES**

All sealing devices shall be of suitable materials which will not be adversely affected by the hydraulic fluid. Whenever possible, sealing devices shall be of the pressure sealing type. Sealing devices on reciprocating or rotating shafts shall prevent all leakage, except that required for lubrication of such devices, under all working conditions, without damaging shafts. Anti-extrusion back up rings shall be used and/or clearances in sealing glands shall be limited to prevent extrusion of the sealing material.

### **DEVICES FOR CIRCUIT CONTROL, PROTECTION AND SAFETY**

#### **Over-pressure capabilities and protection**

Suitable type pressure valves shall be provided on the discharge side for pumps and over pressure protection shall be provided elsewhere in circuits where damage to the equipment or hazards to personnel may result if design pressures are exceeded: Check valves shall be provided on the discharge side of all pumps to prevent any back flow. Sequence control shall be primarily governed by mechanically actuated limit switches, electronic timers, pressure switches, sequence valve or any other position sensing device. All pressure and flow controls shall be designed so that they are adjustable at the system working ranges. A pressure check point shall be provided with each pressure control valve.

## **Interlocks**

The machinery and all connected equipment shall be brought to a safe stop upon failure of electric power, control power, hydraulic power, or control components. If an unscheduled stop would result in an unsafe condition then the failure shall be announced by alarms with the system kept in safe condition. Systems shall remain inoperative after restoration of service until controls are reset. Where there is more than one hydraulically or manually controlled device on any industrial equipment, whereby possible damage or personal injury may be caused by the failure of any one device to function properly, the circuits shall be arranged with protective interlocks. Means shall be provided to prevent uncontrolled movement of hydraulic actuators in all portions of the equipment cycle including pump starting and idling. Electrically and pneumatically controlled hydraulic devices shall be applied in such a manner that in the event of electrical or pneumatic circuit failure

There will be damage to the equipment or danger to personnel. Protection of electrical devices shall conform to appropriate plant electrical standards and shall be completely isolated from coolant, oils and dirt.

## **FLEXIBLE HOSE ASSEMBLIES**

Flexible hose assemblies shall not be constructed from hoses which have been previously used as part of a hose assembly. Flexible hose assemblies shall fulfill all performance requirements specified in the appropriate European and/or International standard(s). Recommendations on storage time for the flexible hose assemblies given by the hose manufacturers shall be considered. Considerations should be given to recommending a service life for hose assemblies.

## **Installation**

Installation of flexible hose assemblies shall:

- have the minimum length necessary to avoid sharp flexing and straining of the hose during the component operation. Flexible hoses should not be bent with a radius smaller than the recommended minimum bending radius
- minimize torsional deflection of the hose during the installation and use, e.g. as a result of a rotating connector jamming

- be located or protected to minimize abrasive rubbing of the hose cover
- be supported, if the weight of the hose assembly could cause undue strain.

If the failure of a flexible hose assembly constitutes a whiplash hazard, it shall be restrained or shielded. If the failure of a flexible hose assembly constitutes a fluid ejection hazard, it shall be shielded.

## **INTERCONNECTING PIPEWORK**

### **GENERAL**

These instructions cover special aspects regarding design construction and commissioning of interconnecting pipe work for hydraulic power systems. For general instruction refer to General Specification for Pipe work which includes also the Piping System Material (PSM).

### **PIPING DESIGN & SIZING**

#### **Design Considerations**

The hydraulic pipe work shall conform to the piping system material PSM prepared for the specific project or to general specification for pipe work which is developed on the base of international codes (ASME-ASTM-DINSAE-CETOP).

All hydraulic interconnecting piping systems shall be designed for a nominal working pressure of 20 per cent above the normal working pressure. Indicative maximum span between supports shall not exceed the indication of the following table unless otherwise indicated in the piping documentation:

<b>Outside Diam. (mm)</b>	<b>6 ÷ 8</b>	<b>10 ÷ 20</b>	<b>20 ÷ 50</b>	<b>Over 50</b>
<b>Max Span (m)</b>	1.0	1.5	2.0	3.0

Pipe clamps to be in any case installed at line ends and before and after change of direction. Piping between actuating devices and control valves shall be as short as possible and rigidly mounted to eliminate vibration. Pressure gauges or gauge connections shall be

supplied at test points between major system components as follows: on power unit; between directional controls and actuators; and at other points where pressure change. Test points shall be indicated in the hydraulic diagram and in the assembly drawings.

### **Pipe sizing**

Interconnecting pipes shall be sized on the basis of technical and economical velocities taking into account the following parameters:

- pressure
- pressure drop
- absolute roughness of pipe
- type of service

Velocity of hydraulic fluids in steel pipes should not exceed generally the following values:

<b><u>SERVICE</u></b>	<b><u>PRESSURE (bar)</u></b>	<b><u>VELOCITY (m/s)</u></b>
Suction lines	All	1
Return lines	All	3
Delivery lines	up to 50	4
	50 ÷ 100	4.5
	100 ÷ 150	5
	150 ÷ 200	5.5
	200 ÷ 400	6

The normal practice is to guarantee a maximum pressure drop of 1.0% of the operational pressure at user T.O.P.

Suction lines shall be sized in order to guarantee the pumps required NPSH. Higher velocities are normally accepted for larger pipe size and for short branches.

### **MATERIALS AND DIMENSIONAL STANDARDS**

Carbon steel pipes and butt weld fittings are supplied pickled clean and free from oxide scale and carbon deposits, neutralized, phosphated and oiled inside. Pipe ends shall be fitted with plastic

caps in order to avoid oxidation during transportation and storage at site. The plastic caps must be visible.

Stainless steel pipes and fittings are supplied not oiled but thoroughly clean and free from dirt. Socket welding fittings are normally supplied black and prior to fabrication need to be thoroughly cleaned inside to remove oxide and debris.

If necessary batch pickling has to be used to eliminate oxide following the instruction submitted.

For piping material specification refer to the Piping System Material (PSM) prepared for the specific project or to General Specification for Pipe work. In any case, all the piping material for hydraulic pipe work shall be stored in site with particular care in order to avoid re-oxidation and contaminations.

Stainless steel material shall be kept in segregated storage areas far from carbon steel materials.

Each piping component has to be inspected prior to fabrication and if needed accurately cleaned or pickled following the instruction given.

### FABRICATION AND ERECTION

Interconnecting pipework shall be installed following the project erection documentation and the general instruction. The erection contractor shall check in advance the erection documentation with the foundation and the final position of the equipment before starting the spool drawing preparation and any fabrication activity.

Pipe fabrication will be performed in dedicated clean area. For field fabrication it is recommended to erect temporary barriers.

Prefabrication of the greatest number of pieces in workshops is advisable. Pipes should be kept covered both before and during their assembling upon the installation completion.

When butt welded fittings are used, welds should be made reasonably accessible also from inside of the pipes, in particular for large diameters. This will allow mechanical cleaning. When socket weld fittings are used, it's imperative to deburr the pipes and provide for a mechanical cleaning or pickling and passivation.

The piping assembly must be carried out accurately. Carefully free the pipe from all burr, inside and outside. When dealing with cutting ring or special fittings, follow the instructions given by the manufacturer. When laying pipelines having long stretches without connected fittings, keep the maximum commercial length of the pipes. Connecting pipes must not hinder the accessibility to the instruments, especially where there are hand controls for

adjustment or tuning devices for checking. When the piping is higher than the hydraulic ports, install bleeders for venting. In case of sag provision for drainage shall be foreseen. An adequate number of disassembly fittings must be installed (flanged joints, and pipe unions etc.) to allow flushing and testing.

Before proceeding to the installation of manifolds, look into the single components to make sure there are no foreign bodies.

During hydraulic pipe assembly, care must be taken when performing cold bending. Do not cut or make holes using a flame cutter. When cutting pipes, use cutting disc type shears and after each cut, deburr and blow the machined piece, or even better use rotating wheel pipe cutter. For large size pipes, where the use of a flame cutter is unavoidable, it's essential to grind and deburr the cut, both externally and internally, taking care to blow and perfectly clean the piece.

For butt welding connection adequate leveling according to piping specification must be executed.

Carbon steel pipes and fittings for hydraulic systems are generally supplied pickled, passivated and oiled. In order to avoid oxidation of joints the first welding must be executed with TIG procedure (Argon gas). This way to proceed avoids the need of further pickling. All pipes and fittings shall be consequently thoroughly inspected before and after fabrication. If some pipes, fittings or spools are found with oxide it has to be pickled again (pickling in tanks) following the instruction given. The disassembled pipes shall be cleaned with proper means (brushes, Tampons, compressed air, wooden mallets, etc.) to eliminate any foreign matter or considerable scaling.

After fabrication and prior to assembly, close the ends of the fabricated and cleaned parts with plastic plugs sealed with adhesive tape, in order to prevent foreign matters or humidity from penetrating. Assemble all prefabricated or on-site manufactured pipes together with all the fittings and valves required for the circuit but do not secure them tightly. This ensures the circuit completion and correctness and allows any necessary correction to be carried out. Finally assemble on site all parts and protect the exposed ends. Piping shall not be placed in a location on the machine where it will interfere with the adjustment, repair or replacement of controls or units.

Piping connections shall be readily accessible for maintenance.

All piping shall be securely supported to avoid vibration or movement. Pipe and tubing lengths between supports shall be as per erection documentation. Piping shall not be welded to

supports. After assembly a thorough inspection will be carried out on the piping system to check eventual re-oxidation phenomena. If during final inspection of the fabricated and erected interconnecting pipingsome parts are found rusty then an in line pickling shall be performed.For the pickling procedure refer to Special instructions for in sitepickling. The final inspection will be carried out also for the on board piping in order toavoid any possible contamination.

## **TESTING OF ERECTED PIPING**

The pipe work as erected shall be hydraulically tested according to design requirements.

The hydraulic test shall be carried out using a fluid type compatible with theselected final working fluid.The hydraulic test pressure shall be 1.2 times the working pressure unlessotherwise indicated on the project documentation.Immediately after the hydraulic test, dismantle the fittings used for test andprepare the circuits for the commissioning.If flushing will be carried out in a further phase, the line shall be drained, driedand filled with dry nitrogen at 1.2 barg pressure.

## **COMMISSIONING**

### **Circuits preparation**

Facilities are normally foreseen in the piping design to facilitate flushing andcleaning connections. It is necessary, during the flushing and cleaning operation,to bypass components such as valves and cylinders. The Contractor has tocheck the erection documentation and to foresee all the necessary temporary fittings and blind flanges for the flushing circuit preparation. The flushing operation shall normally include also on board piping up to the flexible hoses connecting the hydraulic cylinders which have to be by passed on this basis the Contractor has to provide an operating sequence of how they propose to flush the system. The Contractor has to provide authorized personnel with a markedcopy of the system schematic, showing where connections for flushingequipment will be installed. Information on how the system is to beinterconnected to form a continuous loop must be shown on these drawings.Prefabricated loops must be precleaned. All potential trouble spots where dirt may accumulate are to be identified for special attention. All valves, manifolds, cylinders,

system pumps and system reservoir must be bypassed during flushing and capped to prevent entry of dirt. The design of the flushing circuit must include provision for reversal of flow.

Contractor must furnish its own flushing pump; system pumps are not to be used. Pump flow must be high enough to create turbulent flow in every part of circuit during the cleaning phase. This level is to be determined by the following formula, assuming Reynolds Number (Re) to be greater than 10,000 (minimum fluid velocity,  $v$ , m/sec):

$$Re = \frac{Q}{d \times v} \times 1000 \quad (\text{Where: } Q = \text{flow (lpm)} \quad d = \text{pipe ID (mm)} \quad v = \text{kinematics viscosity of the fluid (cSt)})$$

The pump will most likely not be able to maintain the turbulent flow during the fluid flush phase. Flow can be maximized by circuit isolation during this phase. Sampling ports must be provided to permit samples to be taken ahead of filters when flushing in either direction (fluid sampling containers according to ISO 3722). The Contractor and Danieli authorized personnel must agree beforehand as to when and where samples are to be taken. Because of danger and flaking, no rubber hoses are to be used for bypass during flushing. Where flushing all piping in series is not practical because of pressure drop, temporary manifolds may be installed with isolation valves to form parallel circuits. However, the indicated turbulent flow velocity must be guaranteed.

Filters must be provided in order to detect "dirty" conditions; these filters must not be fitted with bypass valves. Isolation valves must be provided so that filters can be changed without disturbing flow. To facilitate the choice of the flushing pumps refer to the table here below. The Flow rates refer to the various internal diameters of pipes assuming  $Re > 10,000$ , Fluid Velocity  $> 4$  m/sec and Fluid Viscosity = 3 cSt.

Pipe ID (mm)	Viscosity (cSt)	Density (kg/m <sup>3</sup> )	Minimum Fluid flow (lpm)	Re No.	Pressure drop (bar/m)
103	3	900	10	10,710	16,16
203	3	900	22	10,379	4,6
303	3	900	30	10,710	2,02
403	3	900	40	10,710	1,5



203.	9..	36.	10.19.	0,96
12,23				
3.3.9..	40.	10.710	0,7.	10,72
4.	3.	9..	08.	10.271
0,24				
7,7.				
0.3.	9..	70.	10.710	0,13
70	3.900.90.		10.342	0,7
8.3.	9..	1.400.	12.384	0.04
4,74				
100	3.900.	2.200.	10.068	0,34,67
1203.900	3.000.19.814			0,24,76
100.3.900	0.000.23.088			0,24,72

### Hydraulic systems flushing preconditions

The Contractor shall supply all the auxiliary devices such as tanks, pumps, filters, valves, manifolds, thermal heaters, temporary bypasses and whatever required for proper field operations. It is a Contractor's responsibility the fluid handling and disposal.

The Contractor must provide assurance in writing that all spent chemicals will be properly disposed off, including used filter cartridges. Customer Environmental Control Department must be involved at this point.

All services to be provided by Customer to Contractor, such as a set-aside area, steam, electricity, water, etc. must be agreed upon in pre-bid meeting. The Contractor is expected to provide field test kit for analyzing dirty level in samples. This is to be used in determining when samples are ready to be sent to outside laboratory. All the chemical solutions, fluids, tools and the flushing operative sequence necessary to carry out the operations in the proper way will be charged to the account of the Contractor upon approval of the personnel authorized by Danieli. The Contractor will be held responsible for any problem caused by incorrect operation of the systems due to a not proper cleanliness

### Flushing activities

The flushing fluid capacity to remove particles from the internal surfaces of piping is in proportion to the quantity of energy available as a result of the fluid pipe surface friction.

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During flushing, every welded joint must be hammered with a ball peen hammer for 30 sec. during each phase of the schedule, including reverse flow. Contractor is responsible for any damage caused by hammering. Hammer in the direction of flow. Though vibrators may be used on low spots where dirt tends to accumulate, hammering is preferred. In addition, starting and stopping flow by sudden opening and closing of valves is a good assist.

Reverse flow is required during pickling, passivation and flushing phases, when the hammering is to be repeated in direction of flow.

The particles removed by the flushing should be caught with a filter with a high "β ratio". We consider fundamental that filters of major companies makers are employed and also we do not recommend the use of low finesse filters followed by high finesse filters, as this is not economically convenient.

During flushing, contractor is to inspect lines frequently and to stop flushing immediately if a leak occurs. Flushing fluid must be kept out of customer's sewers.

After system has been drained of all fluids, system is to be purged with dry nitrogen. An authorized personnel is to verify completion of drying, after which system may be refilled with filtered system fluid for that portion of flush schedule.

#### System tank cleaning

Access cover is removed and the inside is swabbed with lint-free cloth. If reservoir is large enough for a person to enter, contractor's worker must wear clean white paper coveralls and white paper boots for manual wiping of inside with lint-free cloth. Safety precautions for entering closed space must be observed. Access cover and new gaskets are to be reinstalled and checked later for leaks.

#### Final approval

Final samples, to be sent to an outside lab, must be analyzed according to ISO, report must be in ISO 4413 code format (expanding the code to three ranges correlating to 1 μm, 0.5 μm and 0.1 μm). Minimum three samples for each loop circuit may be taken at any time after flushing begins with system fluid and after welded connections have been hammered during this part of the schedule. If clean enough, sample may be drawn for transport to outside lab. This sample is to be drawn by authorized personnel.

While test results are awaited, flushing is to continue. If sample

turnaround is longer than 8 hrs authorized personnel may waive testing by outside lab and agree to use of field test kit or field portable contaminated monitor and related reports (min. three reports for each loop circuit).

If sample results are within specifications (see par, below), flushing may stop and system can be drained. The Contractor will dispose of this contaminated fluid.

The target cleanliness level for systems must be:

Type of system	Contamination Level ISO εεεε- (Target) 2μm-10μm-10μm	FILTER ABSOLUTE FINENESS SUGGESTED Bx≥100
Hydraulic systems with Servo valves	10/13/10 (NAS ε)	1÷2
Hydraulic systems without servo valves	17/10/12 (NAS 6)	3÷0

#### System filling with final fluid

Immediately after flushing is completed, all system components are to be reconnected after contractor's equipment has been removed.

In the case of flushing in which is used the same working fluid, this must be checked by the fluid Manufacturer before the filling on the following characteristics:

viscosity, acidity (T.A.N./S.A.N.)(Total Acid No-Strong acid No.)and water content. In case of these values are not into the range of new product, the Contractor must recondition or change the fluid. Before proceeding to fill-up the system, make sure that the fluid corresponds exactly to the requirements of the design.

All fluids on the market, with no exception, even the new ones and those contained in sealed container, are not perfectly clean. They should, therefore, be filtered.

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Before proceeding to fill-up the tank, check accurately the tank cleanness. Filling must always be done through the appropriated external filter which has a better degree of absolute filtration as the ones mounted on the system. Be extremely careful of any accidental introduction of pollutants, dust, rags and various objects. Test perfect sealing and perfect functionality of the air filters mounted on the vents which permit the intake and emission of air as the level of the fluid rises and drops in the tank. Never mix fluids of different types or makes. If the hydraulic circuits are not immediately filled up with the final fluids all the lines shall be drained, dried and filled up with dry nitrogen at 1 ÷ 2 barg pressure.

### **SAFETY AND ACCESSIBILITY**

All equipment shall be protected against falling objects and operator's accidental movements from material handling and moving equipment as well as excessive temperature and detrimental effects such as water, scale, acid, dirt, dust or other environmental conditions. Automatic controls shall be located and protected to prevent accidental operation. Piping shall not be used to support directional valves. Hydraulic systems provided in the vicinity of open flames high temperatures, molten metal etc. (such as those for furnaces, cranes, coils etc.) special protection shall be given to prevent breakout of fire in case of pressure breakout of the hydraulic fluid. These shall include selection of suitable seal, packing and fittings. Thermal insulation shall be provided for hydraulic systems operating in areas of high temperatures (> 100 °C).

Bladder or piston type gas accumulator shall be charged with nitrogen. Manual on-off valves shall be supplied at each valves stand on pressure line, non-return valve in return lines for safe isolation during maintenance.

Valves and other controls shall be mounted preferably on blocks or valve stands or on the related power unit.

Meter out flow controls shall be used except where high intensification may occur.

An emergency stop shall be provided and shall be readily accessible from the operator's normal working position.

Means shall be provided to prevent rapid vertical drop or inclined slides or rams of equipment when hydraulic power is shut-off in case of operation on vertical or inclined slides or ramps. All components should have a nameplate, standard symbols and item numbers same as drawing.

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## **INSPECTION AND TESTING**

Hydraulic systems, inspections and testing shall conform to General Specification for Quality Control.

## **DRAWINGS AND OTHER DOCUMENTS**

### **DEFINITION OF ENGINEERING PHASES**

#### **BI = Basic information**

It consists in the definition of basic requirements in terms of quality and quantity of fluids consumed by the users.

The data given during this phase are subject to confirmation during the following phases.

#### **BD = Basic design**

It consists in the definition of systems configurations. During this phase a complete check of process requirements of each plant unit has to be completed.

#### **DD = Detail design**

It consists in the development of construction engineering and it allows purchasing of components from the market and consequent fabrication and erection of the piping systems.

Drawings and documents for hydraulic discipline shall conform generally to ISO 1219 standard.

## **GENERAL**

Following the instructions of this general specification the pickling activity on site should be avoided. In the case some pipes or fittings or the entire system require pickling the following procedures can be taken as reference.

It is in any case recommended to subcontract the pickling activities to specialized company.

## **CHEMICAL PRODUCTS TO BE USED FOR PIPES PICKLING OPERATIONS**

There are many methods to perform the pickling operation, the simplest method recommended is, however, to use products

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“ready to use”, such as BETONA or RIDECA.

These products do not require any preparation or particular knowledge for their use, as they offer the advantage of performing the pickling in a single operation. If these products are not available, it is recommended to have the pipes pickled by a specialized company, anyway taking care that, after the inhibited acid solution, passivation must be duly performed; the following products (or similar) to perform the pickling and neutralization/passivation of pipes are suggested

- PRST at 50°C for degreasing
- Lutensol-ON-BASF (chemically pure) for degreasing
- HCl for pickling
- HF for pickling
- H<sub>2</sub>SO<sub>4</sub> for pickling
- CH<sub>3</sub>COOH for pickling
- NaOH for neutralization
- NH<sub>4</sub>OH for passivation
- NaNO<sub>2</sub> for passivation

The product concentrations depend on the Contractor proposed method.

#### PIPE PICKLING IN TANKS

Generally speaking, pickling will be carried out according to the following operating cycle:

Mechanically clean the pipes and fittings (with brushes, compressed air, wooden mallets, etc...) to eliminate any foreign matter or considerable scaling.

Clean by immersion in tanks containing strongly alkaline or similar solutions suitable to removing grease, oil from the pipes surface. Wash under running water.

Protect the threading or other parts in order not to be attacked by the pickling bath with grease or other acid-resistant means.

Pickle by immersion in tanks containing acid solution.

The duration of these operation will depend on the solution concentration and on the cleanliness of the surfaces, which must be free of scales, calamine and oxide.

During pickling, frequently move the prefabricated sections and fittings to assist the acid action on the surfaces and to remove any gas bubbles which could prevent the solution from coming into complete contact with the metal.

The neutralization treatment shall be carried out with a proper alkaline or similar solution.

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This treatment requires particular care because any acid solution residue would continue their corrosive action.

The passivation treatment shall be carried out with a proper passivation solution.

This treatment prevents rust formation after neutralization.

Apply the spray protection, suited to the flushing fluid, on the inner surfaces of the piping. This type of spray protection prevents internal rust protection and it is insoluble in the flushing fluid. Seal the pipe ends with suitable visible (not transparent) plugs. All the fluids shall be disposed following the local regulation.

### PICKLING IN LINE

Generally speaking, pickling will be carried out according to the following operating cycle:

Prepare the circuit so as to link the delivery lines to the return ones, by-passing all the equipment, valves and users.

Disassemble those pipe parts which cannot be included in the pickling closed circuit for specific system reasons.

These disassembled pipes shall be connected together in separate, provisional circuits.

Pickle with chemical solutions circulating in the pipes by means of a special central unit in compliance with the following operating cycle:

- degreasing with an alkaline or similar solution;
- washing with running water;
- pickling with an acid solution;
- neutralization with an alkaline solution;
- washing with running water;
- neutralization and passivation;
- drying

### IMPORTANT:

If after the drying the system is not ready for flushing, pressurize the inner part of the piping with inert gas (e.g. Nitrogen, Helium), in order to avoid any corrosive action on the system.

The maximum time between Drying and Flushing to avoid the system pressurization with inert gas is 2 hours; at any rate, this interval

must be always approved by authorized personnel.

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## **PICKLING PROCEDURE FOR IN LINE PICKLING**

Following procedure is a suggestion utilizing reagents and items easily to find on the European market and takes in consideration to have all laboratory equipment needed for here below described analysis (to be performed while executing the pickling operation). Any other procedure, different from what described here below, could be still utilized achieving, nevertheless, the same final target.

**Contractor shall provide detailed copy of pickling procedure to Danieli for approval.**

Piping pickling treatment forecasts the performance of here below described operations:

washing by means of water  
washing by means of alkaline solution  
pickling  
passivation  
drying

If at the end of the drying phase the piping has not to be submitted to further treatments (such as flushing operations), next phase will be:  
piping system reconditioning followed by the required fluid filling.

If piping system reconditioning is expected to be made not immediately after the pickling operation conclusion, it is a must to perform an additional operation of lines conservation.

### **Washing by means of water.**

Overall piping must be filled by water that will be flushed by means of the pickling unit pumps. Water will be heated up to 70 °C by means of steam injection during such recirculation. This in order to remove all materials presents inside the piping and not attached to it. Overall flushing circuit will be emptied after 2-3 hours of recirculation, and this fluid shall be stored inside a tank where to evacuate all drains to be sent for disposal.

### **Washing by means of alkaline solution**



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Purpose of this procedure is to remove all oils and greases present inside the piping and to allow subsequent acid treatment to react better against the oxidized layer.

To allow such washing the circuit will be filled by water that will be flushed by means of the same pickling unit. Then following reagents will be proportionated:

-SODIUM HYDROXIDE (NaOH) 1 Kg/cubic meter of water

-TRISODIUM PHOSFATE ( $\text{Na}_3\text{PO}_4$ ) 0 Kg/cubic meter of water

Reagents will be solubilized inside the preparation tank of the pickling unit, this in order to obtain a concentrated solution.

Then, such solution will be added to the water recirculating inside the circuit. This procedure will avoid reagents depositing inside the circuit if not perfectly solubilized

Same procedure will also be performed for any other reagent, even if not recalled, to prepare all chemical solutions foreseen for pickling and passivation operations. Above described adding will make the recirculating solution with the following chemical concentration:

SODIUM HYDROXIDE (NaOH) 1%

TRISODIUM PHOSFATE ( $\text{Na}_3\text{PO}_4$ ) 0,0%

This recirculating solution will be heated up to reach 60-70°C by means of steam injection and it'll be kept in circulation for about 2-3 hours. After this period, this solution will be emptied and the circuit will be washed by water up until removing all traces of alkali, checking the washing water free from any greases or oils traces.

Alkaline washing shall be repeated if in presence of oils or greases traces.

All discharged solutions shall be stored inside a disposal tank.

#### Acid washing (citric treatment).

Purpose of the acid washing is to solubilize the oxide layer present against the inside walls of the piping. When the previous alkaline washing and water washing is concluded, the circuit will be filled by water adding following reagents:

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CITRIC ACID ( $C_7H_8O_7$ )      30 Kg/cubic meter of water  
RODINE INHIBITOR 31 A      1 Kg/cubic meter of water

Ammonia concentrated at 20% will be added up until to have the solution reaching a Ph value equal to 3,0.

Then, this solution will be heated up to reach 90°C by means of steam injection.

Following analysis shall be randomly performed during this heating phase:

- ACIDITY CONTENT;
- FERROUS IRON;
- FERRIC IRON.

Following checking and analysis shall be performed during pickling operation:

- 1) definition of the total circuit volume (by means of the engineering);
- 2) PH checking for the solutions used for piping circulation;
- 3) Acidity content detection;
- 4) Ferrous and ferric ion concentration verification.

With the operations here above described it is possible to:

- a) Verify, through the total volume quantity definition, the quantity of reagents to be deployed to obtain the exact solution concentration to be placed in circulation inside the system and in accordance to the herebelow described specifications;
- b) Check if there is always an active acid excess during the pickling execution needed to solubilize all oxides present inside the circuit;
- c) Define when to stop the pickling operations through the verification of the iron stabilization (ferrous ferric) solubilized by the acid attack.

Washing procedure will be performed up until to stabilize the iron concentration, showing in this way no more oxides to solubilize. By the way, acid washing duration will not be less than 4 hours.

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## Passivation

All oxides present against the inner parts of the piping have been removed once completed the above here-described acid washing, leaving raw the inner parts of the piping.

Leaving the piping in this condition means letting the inner parts of the piping to be subjected to oxidation, with consequent rust formation.

**Purpose of the passivation phase is to create a protective layer on the inside walls of the piping, protecting them from oxidation.** Solution temperature will be dropped down to

60-65°C and citric acid (equal to 0.5% or equivalent to 0.5 Kg/cubic meter) and ammonia will be added to bring the solution PH up to reach 9.5. Temperature for about 1 (one) hour.

Then, sodium nitrite ( $\text{NaNO}_2$ ) in proportion of 0.5 Kg/cubic meter of the solution will be added. Concentration of this reagent will be equivalent to 0.5% so this passivating solution will be kept in circulation for 4 (four) hours keeping the temperature steady. The circuit will be emptied once met this duration.

Once emptied the circuit from this solution, the circuit shall be washed by means of demineralized water, with Ph value equal to 9 adding a bit of ammonia, if there are any doubts about complete removal of this solution (i.e. if sensible volume of fluid is still inside the circuit). Then, the circuit will be emptied once more.

All removed solutions during passivation phase will be stored inside a disposal tank.

Pressurized nitrogen will be blown through the vent pipe to empty the circuit fully, opening and closing all discharging valves alternatively in order to allow gas flow concentration inside all various circuit branches. Next phase to be processed will be the drying operation.

## Drying

Nitrogen will be inserted to empty the circuit as soon as the passivation phase is concluded, opening all drains with a low nitrogen flow and, eventually, opening flanges connection in order to drain the solution as much as possible.

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The moisture still present inside the circuit will be dried by nitrogen insertion heated up by means of suitable heaters. Gas moisture will be measured by hygrometer device at its exit while inserting the nitrogen, that will continue opening and closing alternatively all various circuit branches and up until to have the moisture level reaching a value lower than 2-3%.

### **Piping system reconditioning.**

All temporary piping connection will be reconditioned as soon as the above here described operations, and/or flushing phase has been completed. Particular care shall be taken to avoid piping contamination during such phase. Further phase will be circuit filling with the final fluid.

### **Lines conservation**

Time frame between chemical treatment and further flushing operation, or circuit start up with final fluid, shall be as short as possible to prevent oxidation of inner piping walls.

This is never achievable and the whole circuit shall be kept under a preservation state. The most suitable preservation state is achievable keeping the whole circuit the system will be started up. Then, nitrogen will be inserted inside the circuit up to reach a pressure value of 1-2 barg once the drain valves have been shut. Such value shall be detected through the gauge installed along the circuit. Nitrogen pressure shall be checked 24 hours later to verify there are no leakage out from the circuit as well as the moisture content.

Heated nitrogen shall be inserted in the circuit if the detected moisture content will be higher from the defined value, then, once reached it, the circuit will be pressurized once more.

This checking procedure will be performed on a daily basis for 3 (three) consecutive days and up until this moisture content will remain constant under the stated values. If so, moisture content checking frequency could be performed once every two weeks, and keeping it up to the start up of the system.

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A visual check of the piping condition, removing the flanged joints, shall be performed every 2 (two) months if the nitrogen preservation is forecasted longer than 2 (two) months. A light nitrogen flow shall be kept running through the circuit avoiding air contamination while performing this checking. A biweekly checking shall be performed as above here described once the circuit has been pressurized by nitrogen after this visual check.

Finally, hydraulic system arrangements are very sophisticated, neat and should be supervised very carefully, cleanliness is important in all steps, for piping and equipments, starting from the way of proper storage to the fabrication, assembly and installation otherwise fatal results may be occurred. As I got the chance to supervise these procedures and witnessed these steps in SMI Melt shop erection, I acquired good experience so I liked to share it with the others who have the interest; therefore I submitted this research with the aid of practical and theoretical tools to get the advantages.

Senior Mechanical Engineer  
Mazin Maarouf Nejim

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Eng. Mazin